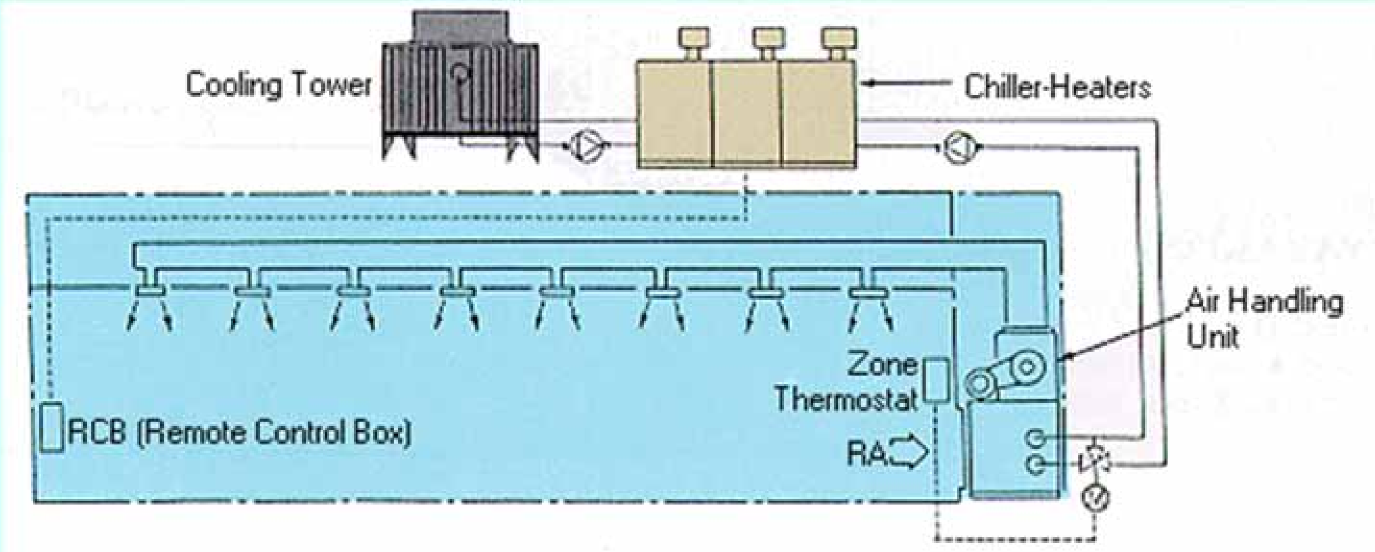
MEBS6008 Environmental Services II

http://www.mech.hku.hk/bse/MEBS6008/



Introduction

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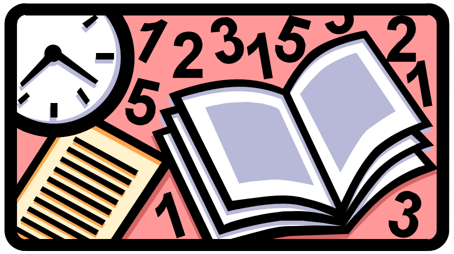
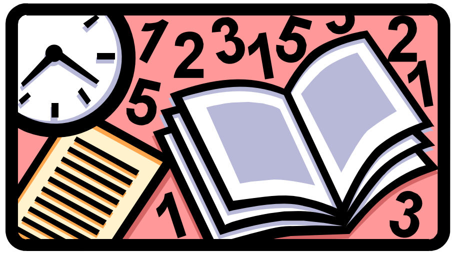
Sep 2012

Background



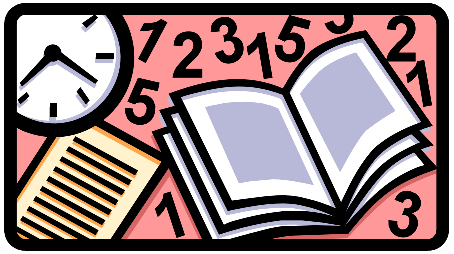
- MEBS6008 Environmental Services II
- Educational Objectives:
  - To introduce students to the important systems and applications of environmental services for more detailed study.
  - To enable students to design appropriate heating, ventilating, air-conditioning and refrigerating (HVAC&R) systems and evaluate their characteristics and performance.

Background

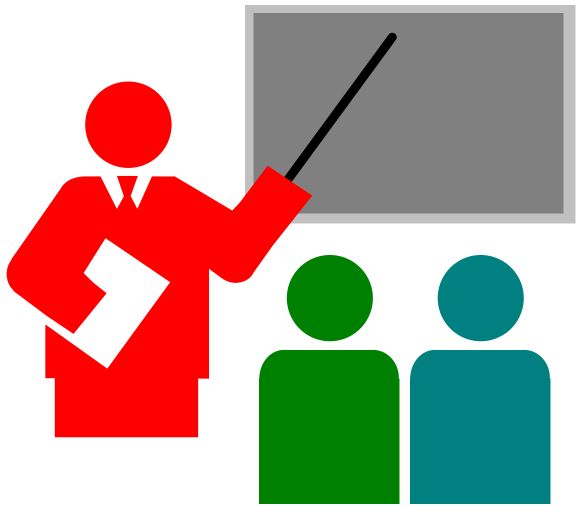


- MEBS6008 Environmental Services II
- Learning Outcomes:
  - To describe the basic principles and characteristics of HVAC systems and components.
  - To develop skills for design of HVAC&R systems and evaluation of their characteristics and performance.
- Assessment: 100% by examination (2 hours)

Background



- Two related courses:
  - MEBS6006 Environmental services I
    - Basic principles of HVACR
    - Practical design skills
  - MEBS6008 Environmental services II
    - System characteristics and operation
    - Analysis and design strategies



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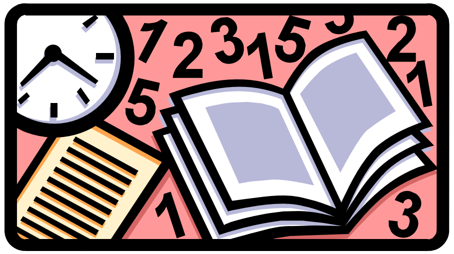

- Study topics of MEBS6008:
  - Fluid Network Analysis
  - Fans and Pumps
  - Space Air Diffusion

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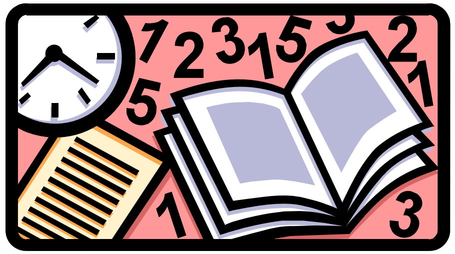
  - Heat Rejection & Sea Water Cooling
  - Thermal Storage Systems
  - Heat Pumps & Heat Recovery Systems
  - Noise & Vibration Control

Dr. Benjamin P. L. Ho

Background



- Recommended references:
  - ASHRAE, 2009. *ASHRAE Fundamentals Handbook 2009*, SI edition, American Society of Heating, Refrigerating, and Air-Conditioning Engineers, Atlanta, GA. [ebook via Knovel][ASHRAE catalog via Techstreet]
  - ASHRAE, 2010. *ASHRAE Refrigeration Handbook 2010*, SI edition, American Society of Heating, Refrigerating, and Air-Conditioning Engineers, Atlanta, GA. [ASHRAE catalog via Techstreet][ebook via Knovel (IP edition)]
  - Wang, S. K., 2001. *Handbook of Air Conditioning and Refrigeration*, 2nd ed., McGraw-Hill, New York. [697.93 W24 h]

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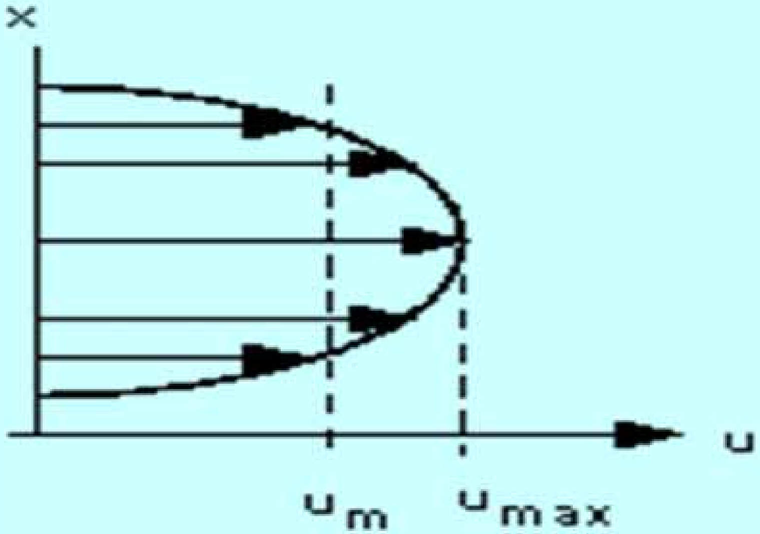

Fluid Network Analysis I

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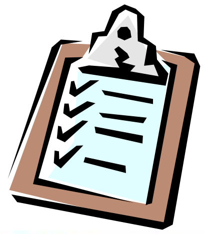
Sep 2012

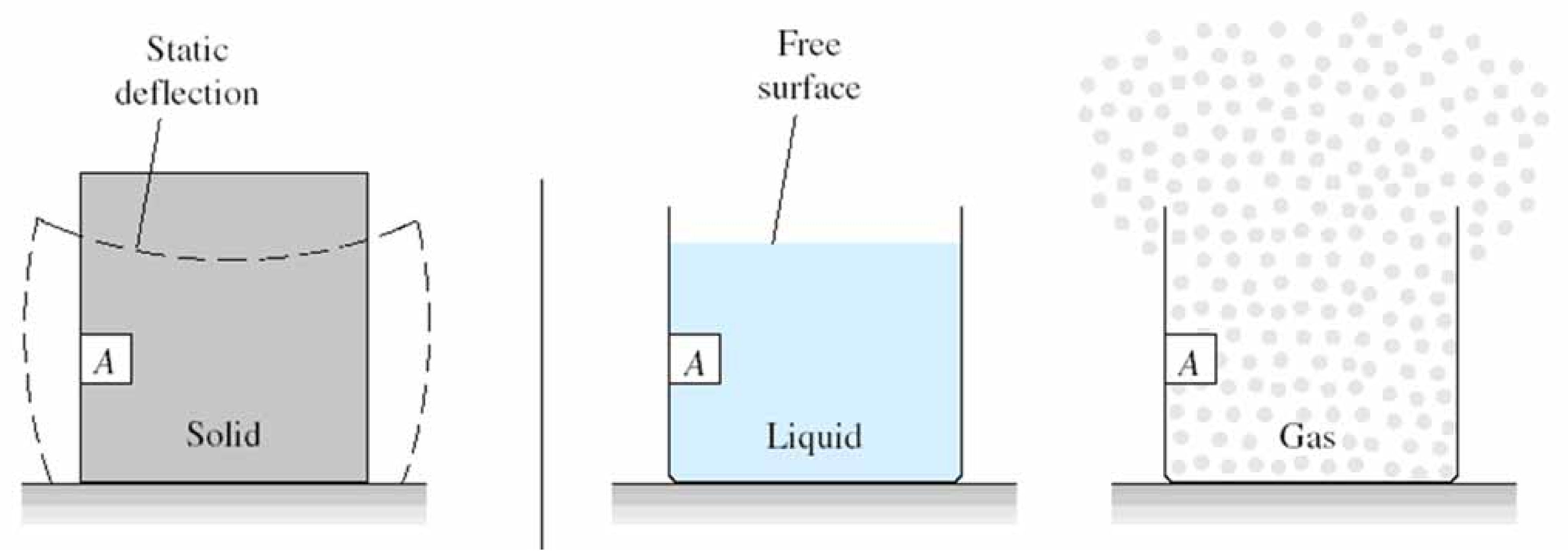
Contents



- Fluid Properties
- Fluid Dynamics
- Basic Flow Processes
- Flow Analysis

Fluid Properties

- HVAC (heating, ventilation & air-conditioning) processes
  - Often involve FLUID flows (e.g. air and water)
  - Understanding of fluid mechanics is important
- Fluid Mechanics – study of fluids at rest, in motion, and the effects of fluids on boundaries
  - Fluid statics
  - Momentum and energy analyses
  - Viscous effects and pressure forces



Fluid cannot resist shear.
Containing walls are needed.

Fluid Properties

- Under shear stress
  - A solid deforms only a finite amount
  - A fluid moves and deforms continuously
- Liquids and gases
  - Molecular actions
  - Degree of compressibility
- Two important properties
  - Pressure (static): $p_1 - p_2 = -\rho g\ (h_1 - h_2)$
  - Velocity (kinematic)

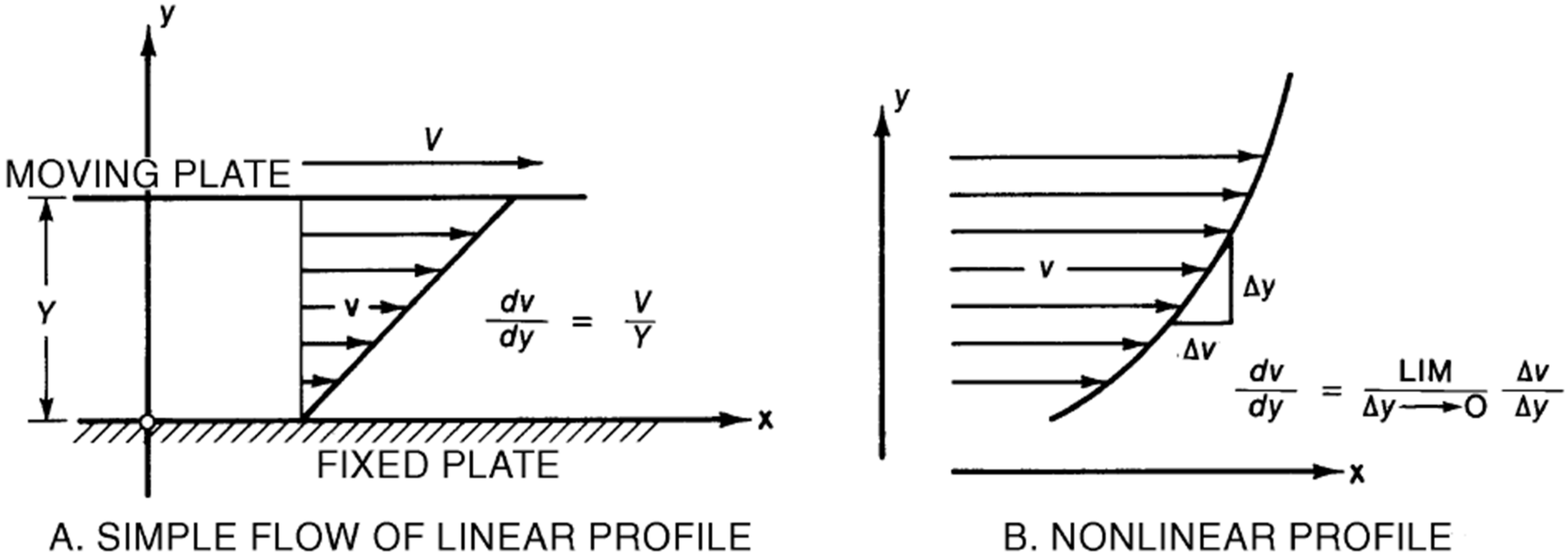
Fluid Properties

- Fluid motion
  - Ideal-fluid model: no resistance to shearing
    - Flow analysis is well developed
  - Real model: effects of viscous action
- Fluids in HVAC applications
  - Most of them are "Newtonian"*
    - Deformation is directly proportional to the shearing stress (Newtonian Law of Viscosity)
  - Viscosity does influence turbulence

* See also http://en.wikipedia.org/wiki/Newtonian_fluid

Fluid Properties

- Common fluid properties
  - Density (ρ): mass per unit volume
    - Density of water = 998 kg/m^3
    - Density of air = 1.20 kg/m^3
  - Viscosity: resistance of fluid layers to shear
    - $F / A = \mu (V / Y)$
      - F = tangential force
      - A = area of the plate
      - V = velocity
      - Y = separation distance
      - μ = absolute viscosity or dynamic viscosity



Velocity profiles and gradients in shear flows

(Source: *ASHRAE Fundamentals Handbook 2001*)

Fluid Properties

- Viscosity in complex flows
  - $F/A = \tau$ = shearing stress
  - V/Y = lateral velocity gradient
  - Therefore, $\tau = \mu\,(dV\,/\,dY)$
- Absolute viscosity (μ)
  - Depends on temperature
  - μ of water = 1.0 mN.s/m^2
  - μ of air = 18 μN.s/m^2

Fluid Properties

- Kinematic viscosity (ν): ratio of absolute viscosity to density
  - $\nu = \mu / \rho$
  - ν of water = 1.00 mm^2/s
  - ν of air = 16 mm^2/s

Fluid Dynamics

- Physical laws for homogenous, constant-property, incompressible fluids
- Continuity: conservation of matter
  - $\int$(density x velocity) dA = constant
  - For constant cross-sectional area,
    - Mass flow rate = $\rho V A$ = constant
  - When flow is incompressible, ρ is constant, then
    - Volume flow rate = $V A$ = constant

Fluid Dynamics

- Pressure variation across flow
  - Variation across streamlines involves fluid rotation (vorticity)
  - Lateral pressure variation across streamlines is given by:

$$\frac{\partial}{\partial r}\left(\frac{p}{\rho}+gz\right)=\frac{v^2}{r}$$

r = radius of curvature of streamline

z = elevation

  - This equation explains
    - Pressure difference between the inside & outside walls of a bend and near other regions of section change
    - That pressure variation is hydrostatic ($p + \rho\, g\, z$) = constant

Fluid Dynamics

- Bernoulli equation *
  - Basic tool for fluid flow analysis
  - Apply first law of thermodynamics
    - $\Delta E =$ Work done (W) + Heat absorbed (Q)
  - Fluid energy is composed of kinetic, potential and internal (u) energies. Per unit mass of fluid, the energy change is:

$$\Delta\left(\frac{v^2}{2} + gz + u\right) = E_M - \Delta\left(\frac{p}{\rho}\right) + Q$$

Fluid energy | External work | Pressure/flow work

* See also http://en.wikipedia.org/wiki/Bernoulli's_principle

Fluid Dynamics

- Bernoulli equation (cont'd)
  - Rearrange the equation,

$$\Delta\left(\frac{v^2}{2} + gz + \frac{p}{\rho}\right) + \Delta u = E_M - Q$$

  - Bernoulli constant = $\pi = \dfrac{p}{\rho} + \dfrac{v^2}{2} + gz$ ← Energy per volume flow
  - Alternative forms:

Energy per mass flow → $$p + \frac{\rho v^2}{2} + \rho g z = \rho \pi$$

For liquid flow (or head) → $$\frac{p}{\rho g} + \frac{v^2}{2g} + z = \frac{\pi}{g}$$

Fluid Dynamics

- Many pipe/duct systems can be considered as "one-dimensional flow"
  - Use Bernoulli equation to analyse velocity and pressure
  - For steady flow, irrotational, incompressible flow,

$$\frac{p}{\rho g} + \frac{v^2}{2g} + z = \text{constant}$$

Pressure head

Velocity head (kinetic)

Potential head (elevation)

Total head

Fluid Dynamics

- If the section-average velocity (*V*) is used, the kinetic energy term of the Bernoulli constant ($v^2/2$) is expressed as ($\alpha V^2/2$),
  - where α = kinetic energy factor (ratio of true kinetic energy of the velocity profile to that of the mean flow velocity)
  - For laminar flow in a wide rectangular channel, α = 1.54; for a pipe, α = 2.0

Fluid Dynamics

- Assume $Q = 0$, Bernoulli equation can be used to determine the change in energy between two stations

External work

Change of internal energy, Δu

$$\left(\frac{p}{\rho}+\alpha\frac{V^2}{2}+gz\right)_1+E_M=\left(\frac{p}{\rho}+\alpha\frac{V^2}{2}+gz\right)_2+E_L$$

- Or, dividing by g,

$$\left(\frac{p}{\rho g}+\alpha\frac{V^2}{2g}+z\right)_1+H_M=\left(\frac{p}{\rho g}+\alpha\frac{V^2}{2g}+z\right)_2+H_L$$

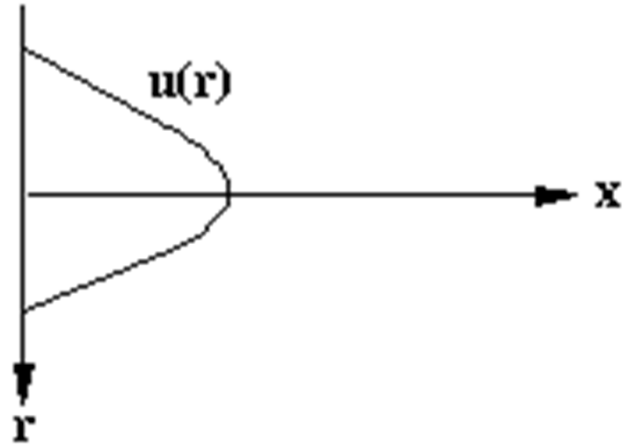
Fluid Dynamics

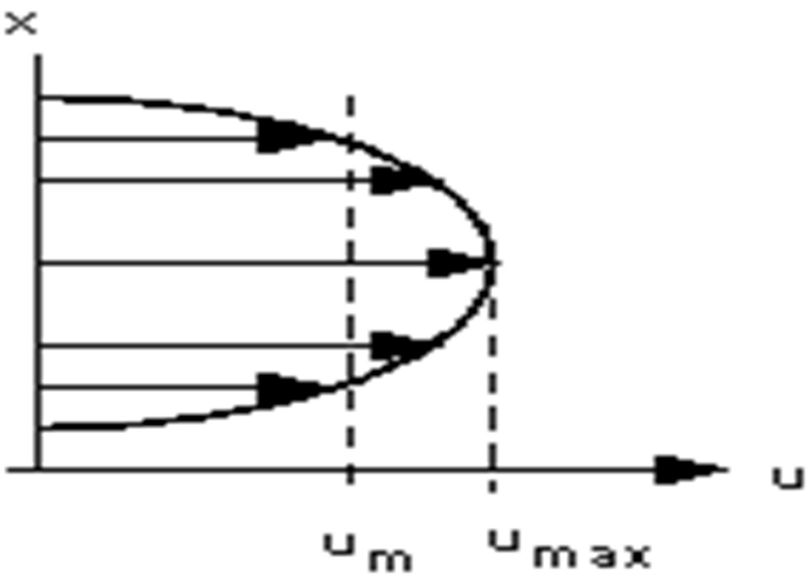
- Laminar flow
  - For steady, fully developed laminar flow in a parallel-walled conduit, the shear stress τ varies linearly with distance *y* from the centerline
  - For a wide rectangular channel,
    $$\tau = \left(\frac{y}{b}\right)\tau_w = \mu \frac{dv}{dy}$$
    - τ_w = wall shear stress = $b\,(dp/ds)$
    - $2b$ = wall spacing
    - s = flow direction
  - Because velocity = 0 at the wall ($y = b$), the integrated result is:
    $$v = \left(\frac{b^2 - y^2}{2\mu}\right)\frac{dp}{ds}$$
    ← Poiseuille-flow parabolic velocity profile

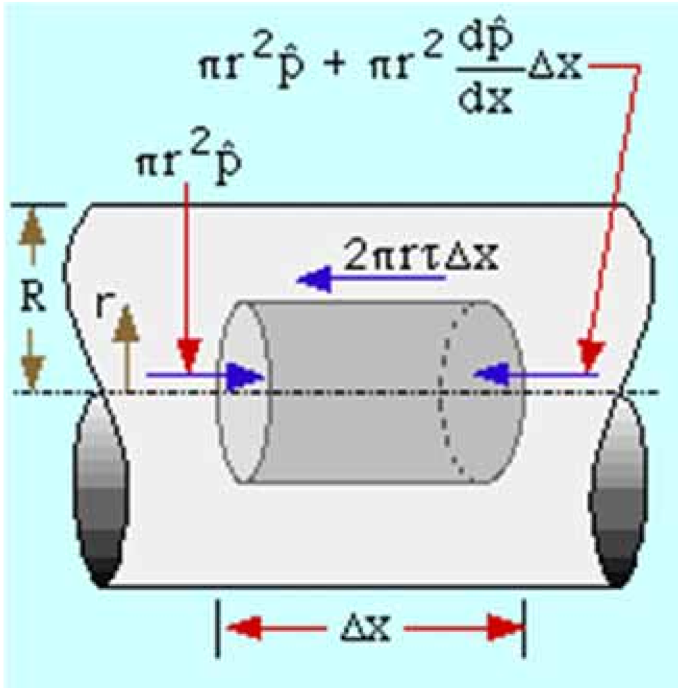
Fluid Dynamics

- Laminar flow (cont'd)
  - Average velocity $V = 2/3$ of max. velocity (at $y = 0$)
  - Longitudinal pressure drop in terms of conduit flow velocity is: $$\frac{dp}{ds} = -\left(\frac{3\mu V}{b^2}\right)$$
  - For axisymmetric conduit (pipe) of radius R, the parabolic velocity profile can be derived. The average velocity $V = ½$ of max. velocity, and pressure drop is: $$\frac{dp}{ds} = -\left(\frac{8\mu V}{R^2}\right)$$


2R
l

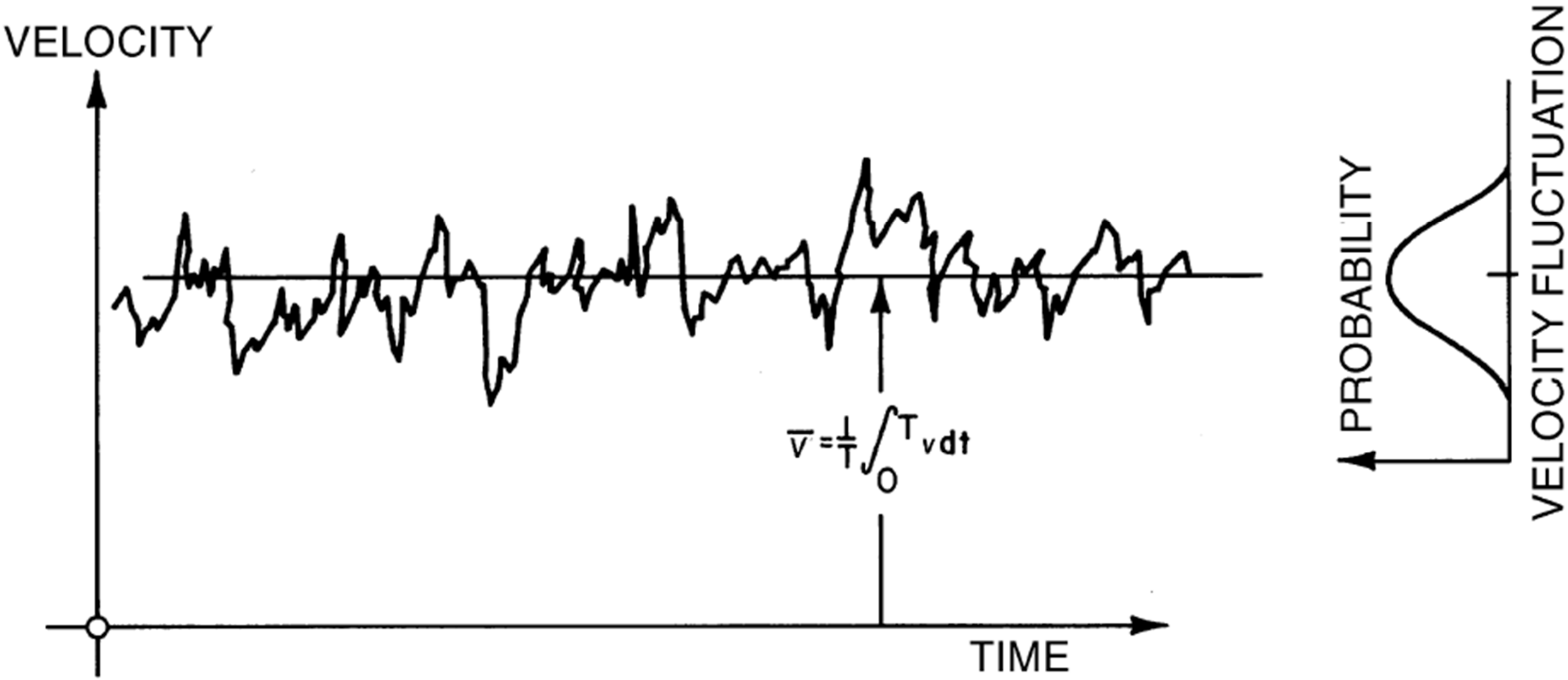

u(r)
x
r


x
u
u_m
u_{max}


$\pi r^2 \hat{p} + \pi r^2 \frac{d\hat{p}}{dx} \Delta x$
$\pi r^2 \hat{p}$
$2\pi r \tau \Delta x$
R
r
Δx

Fluid Dynamics

- Turbulence
  - Random fluctuations of flow (velocity & pressure)
    - Without any order or periodicity
  - Can be quantified by statistical factors
    - "Strength of turbulence" is characterized by the root-mean-square of the instantaneous velocity variation about the mean velocity
  - Effect of turbulence
    - Cause the fluid to diffuse momentum, heat and mass very rapidly across the flow



Velocity fluctuation at point in turbulent flow

(Source: *ASHRAE Fundamentals Handbook 2001*)

Fluid Dynamics

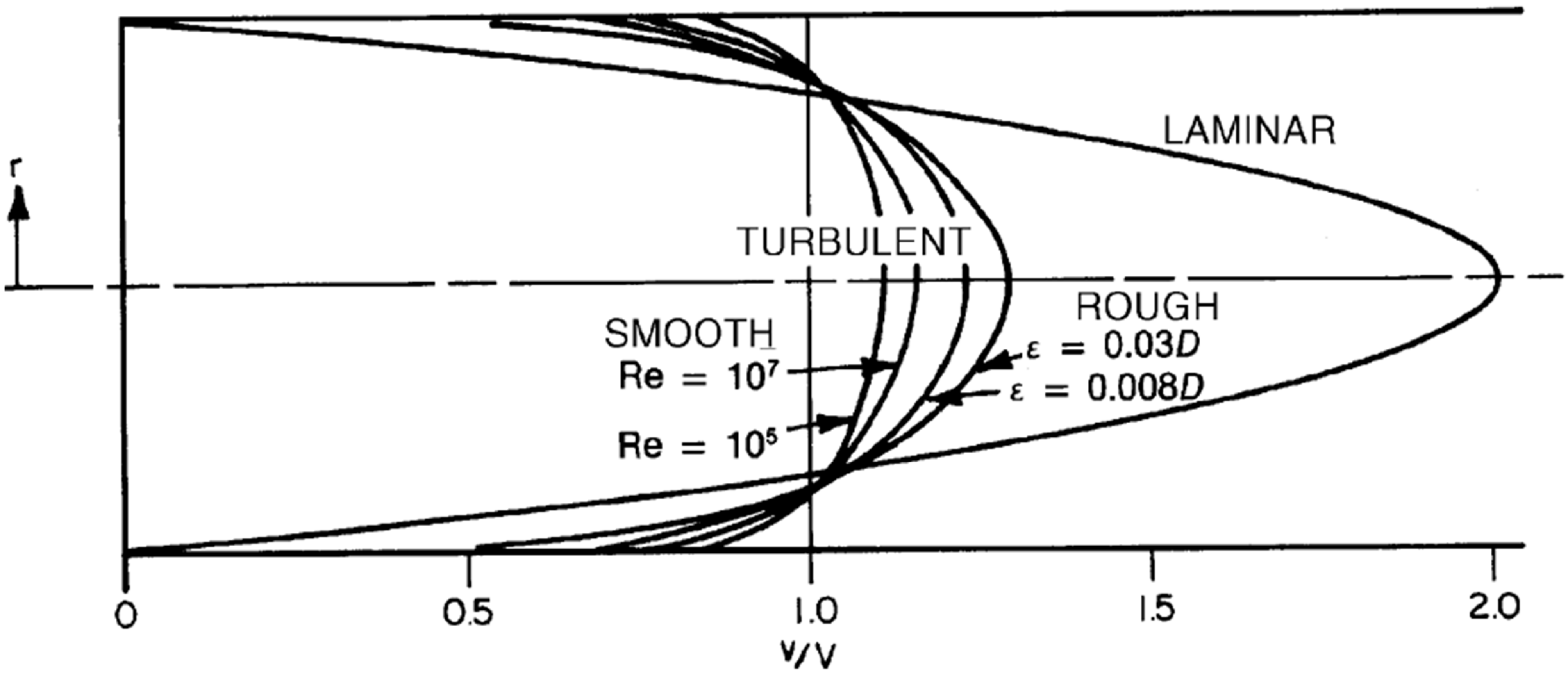
- Reynolds number (Re): dimensionless, gives the relative ratio of inertial to viscous forces
  - $\mathrm{Re} = V\,L\,/\,\nu = \rho V\,L\,/\,\mu$
    - V = velocity of fluid
    - L = characteristics length (For pipes, L = diameter)
    - ν = kinematic viscosity
    - ρ = density of fluid
    - μ = absolute viscosity
  - Laminar flow if $\mathrm{Re} < 2000$; fully turbulence if $\mathrm{Re} > 10000$
  - Transition state if $2000 < \mathrm{Re} < 10000$

Fluid Flow Visualisation

- Video presentation
  - Fluid Flow [video, 24 min.], show how a fluid flows over a solid body
    - Boundary layer, Vorticity, Drag, Unsteady forces, Wave motions
  - YouTube:
    - Slow flow past cylinder - experimental (0:30), http://youtu.be/gbDscDSUAg4
    - Slightly faster flow past cylinder - experimental (0:12), http://youtu.be/vQHXIHpvcvU
    - Flow past cylinder: Karman vortex Street - experimental (0:10), http://youtu.be/CB2aWiesq0g
    - Experimental flow separation (0:37), http://youtu.be/Vjk9Ux2COx0

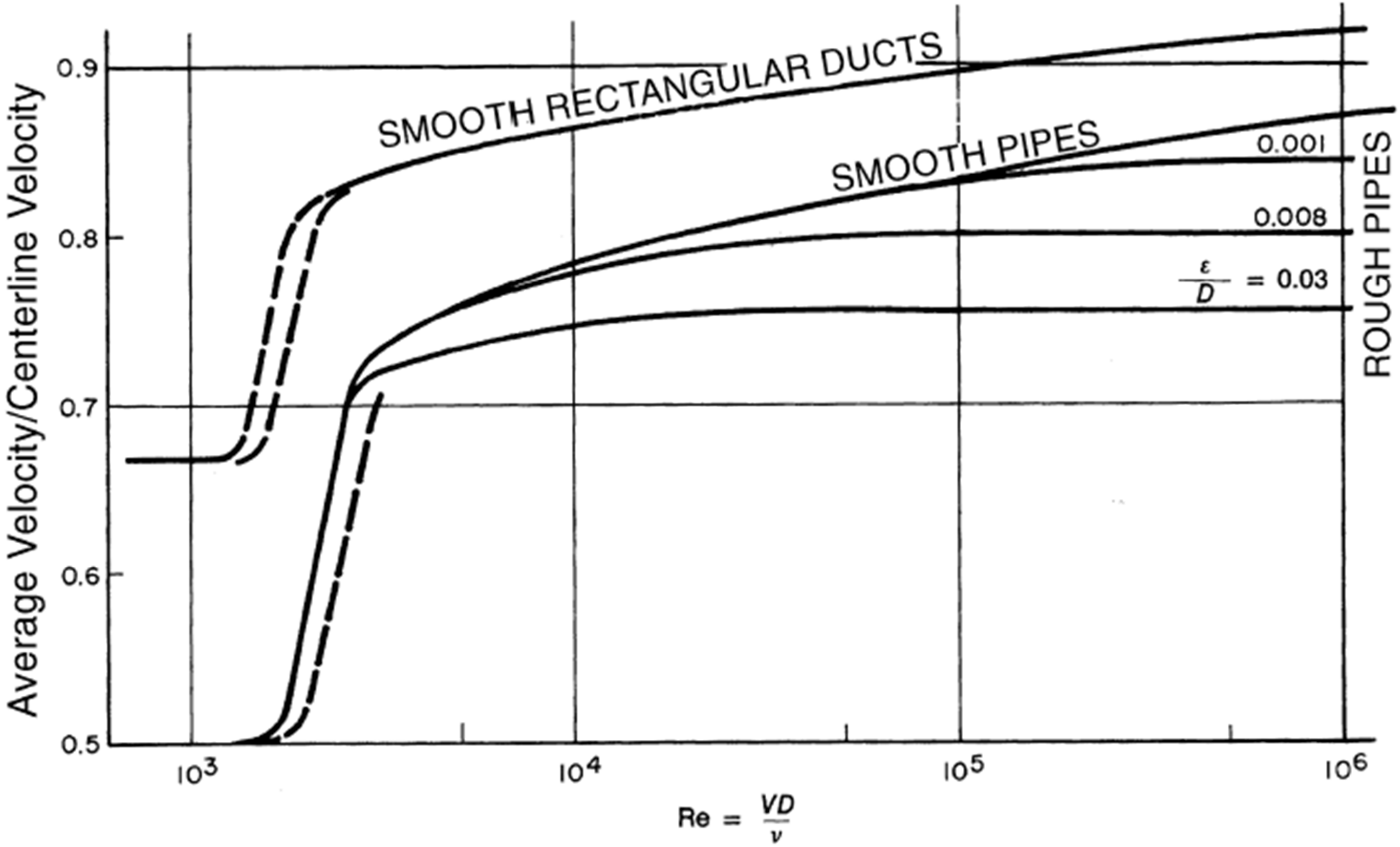
Basic Flow Processes

- Wall friction
  - At the boundary of real-fluid flow, the relative tangential velocity at fluid surface is zero
    - High shear stress near the wall boundary
    - Slowing down of adjacent fluid layers
  - Velocity profiles near a wall
    - Laminar and turbulent flow differ significantly
    - Pipe factor = ratio of average to max. (centreline) velocity



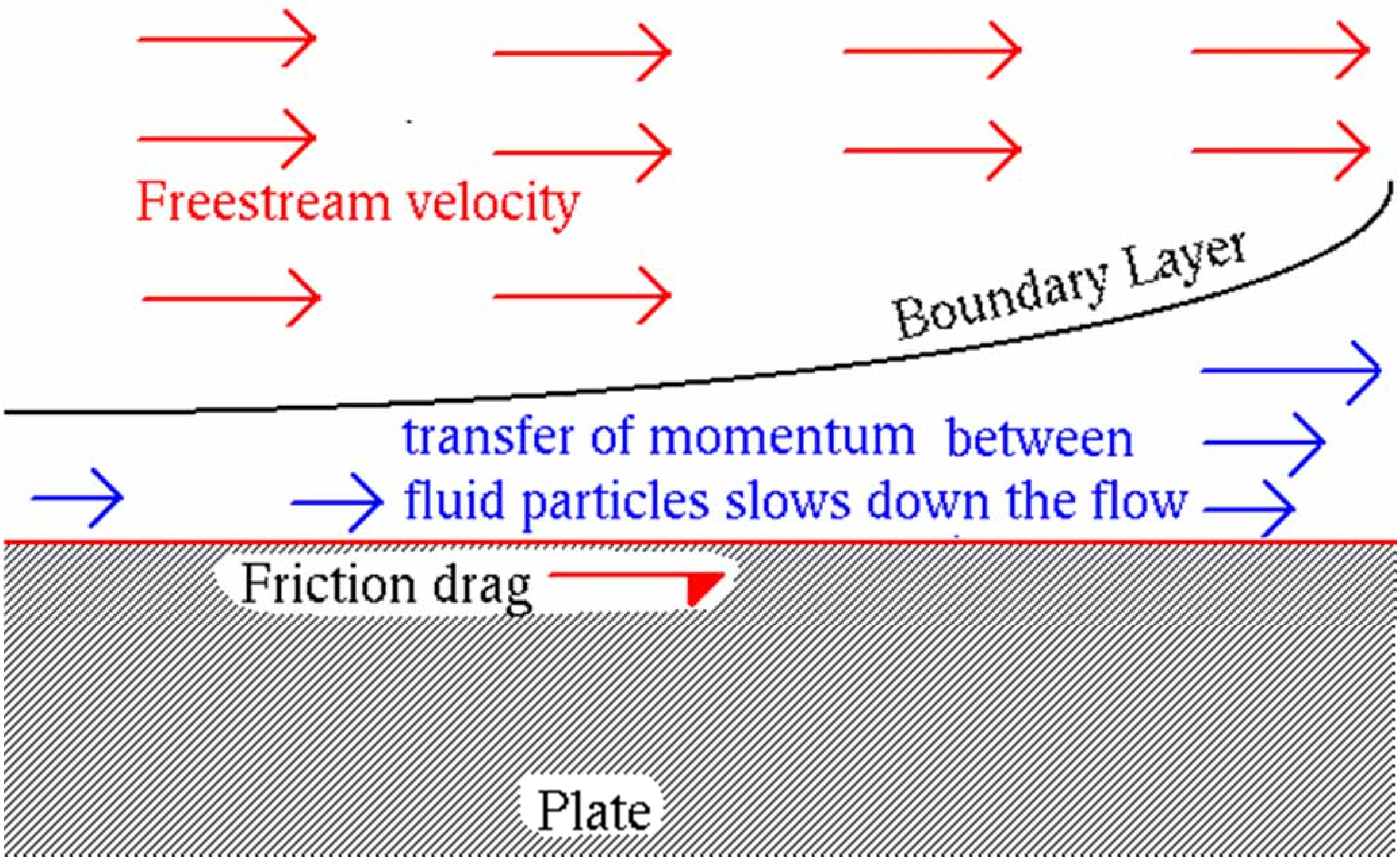
Velocity profiles of flow in pipes

(Source: *ASHRAE Fundamentals Handbook 2001*)



Pipe factor for flow in conduits

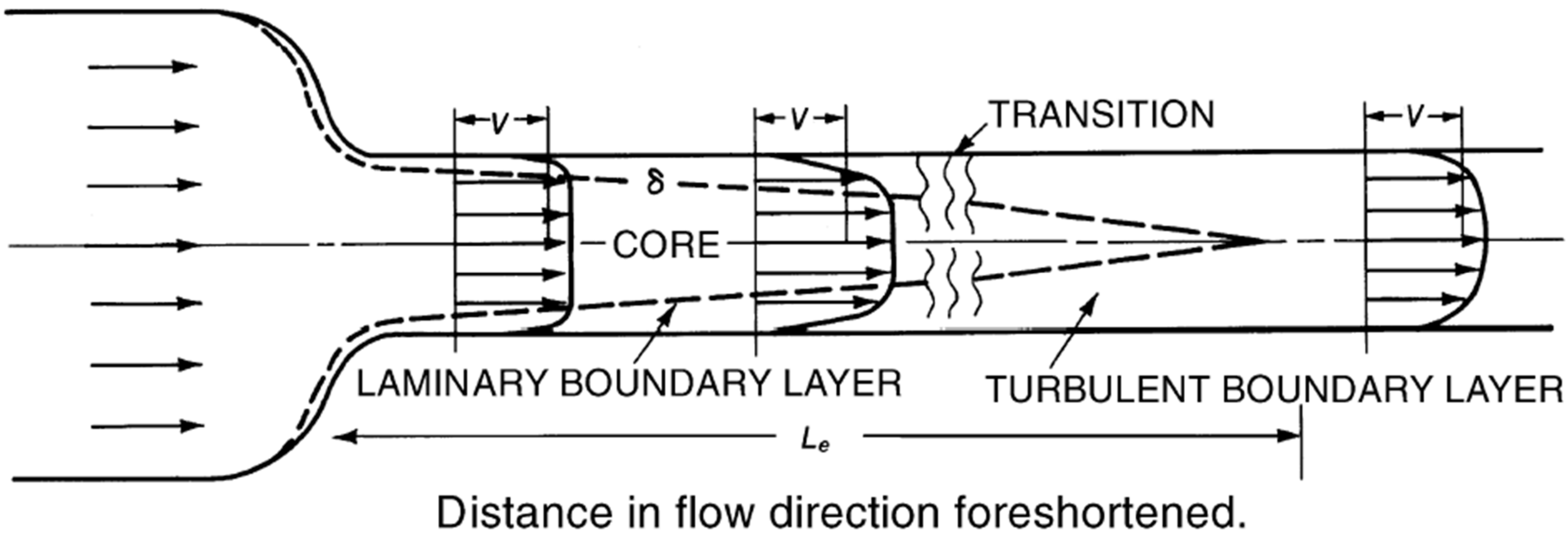
(Source: *ASHRAE Fundamentals Handbook 2001*)



Source: Computer Aided Learning In Fluid Dynamics
(http://cvu.strath.ac.uk/courseware/calf/CALF/index/web_calf.html)

Basic Flow Processes

- Boundary layer
  - Encompasses all viscous or turbulent actions
    - Causing velocity to increase rapidly from zero to that of outer flow edge
  - Generally laminar near the start of their formation, but may become turbulent downstream
  - For conduit flows, pipe diameter is small compared with distances in flow direction
    - Layers from walls will meet at the centreline

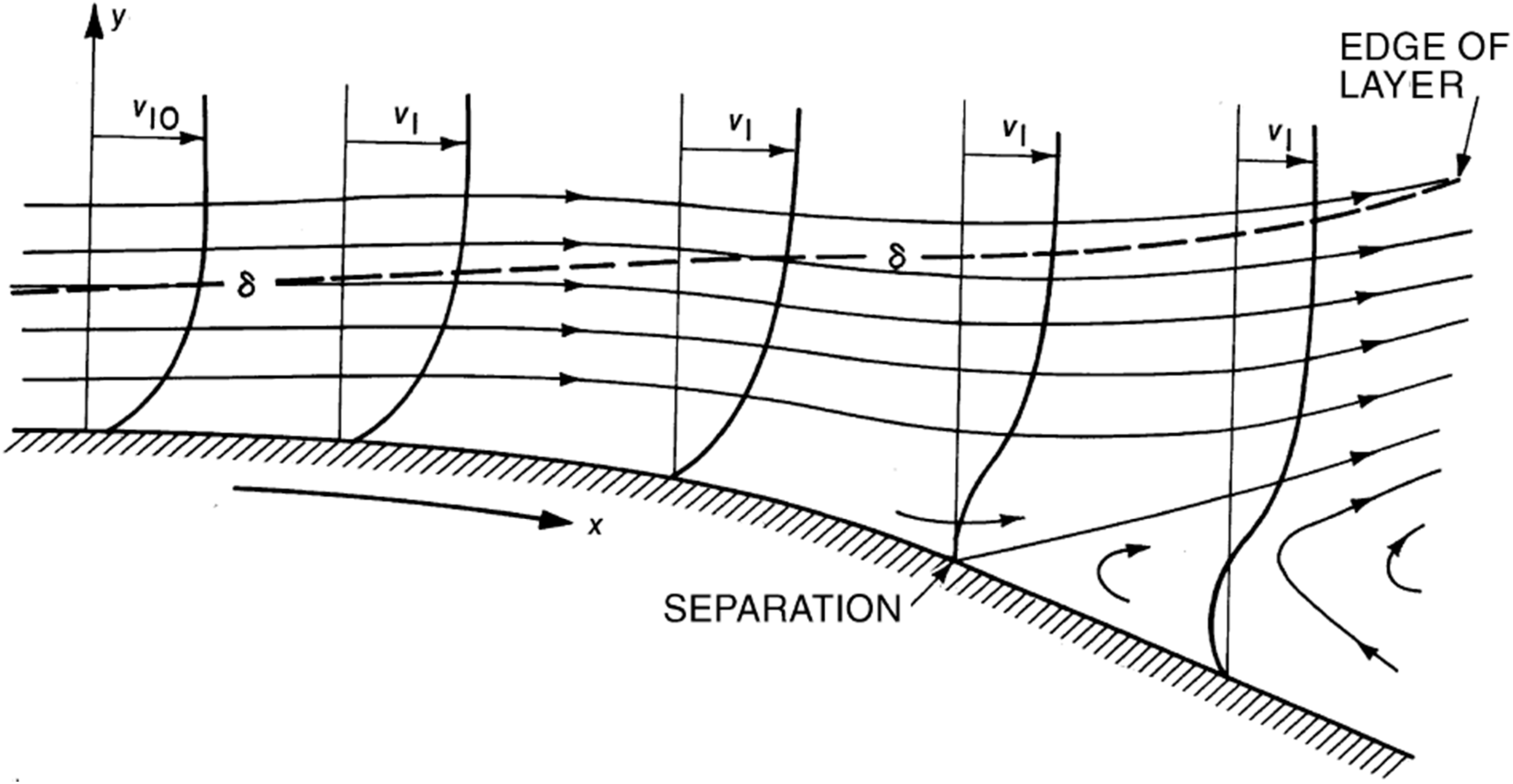


Flow in conduit entrance region

(Source: *ASHRAE Fundamentals Handbook 2001*)

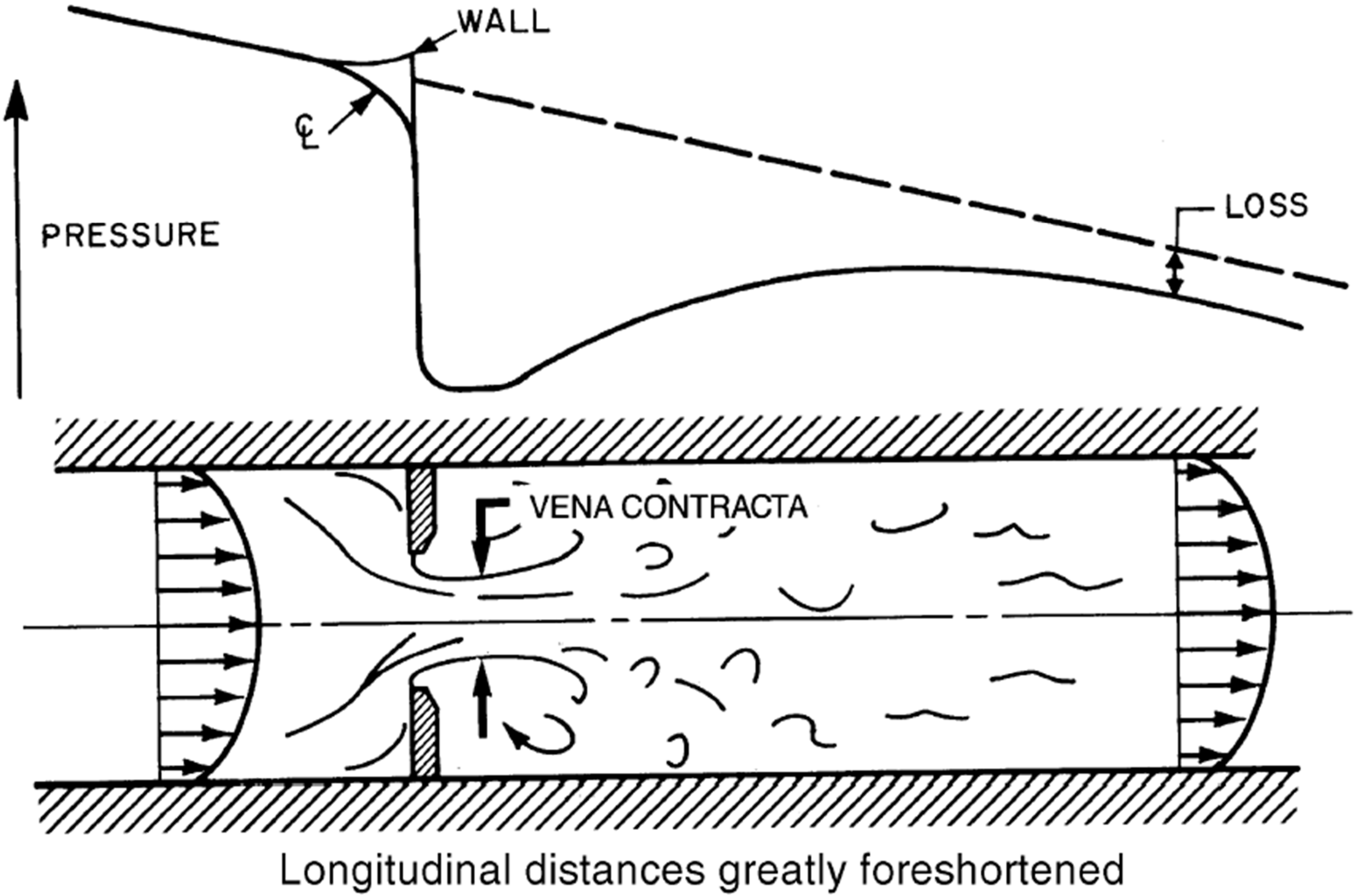
Basic Flow Processes

- In some boundary-layer flows, pressure gradient effects can be severe and may even lead to "separation" (fluid may backflow near the wall)
- Flow separation is due to frictional velocity reduction near the wall (difficult to predict)
  - Dynamic separation (dynamic growth of boundary)
  - Geometric separation (e.g. pass over a sharp corner or sharp entrance or sudden expansion)



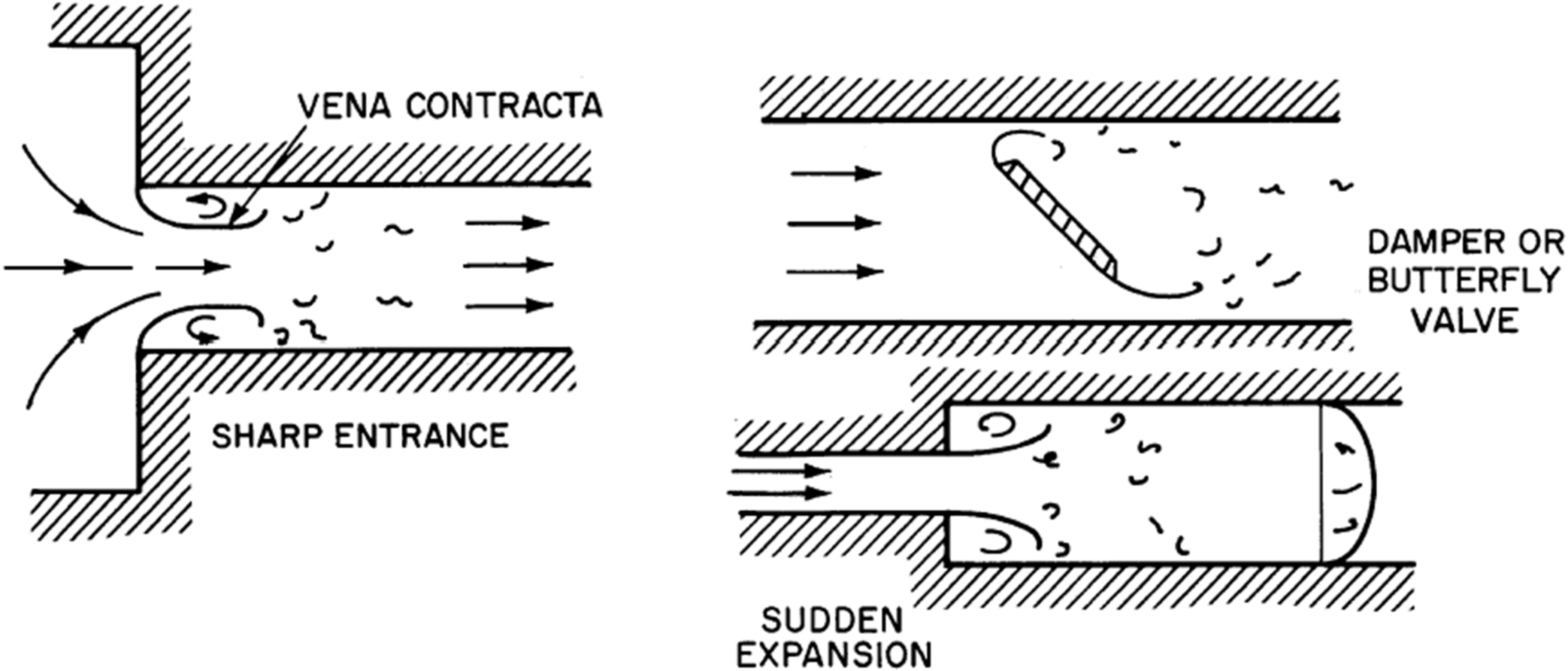
Boundary layer flows to separation

(Source: *ASHRAE Fundamentals Handbook 2001*)



Geometric separation, flow development and loss in flow through orifice

(Source: *ASHRAE Fundamentals Handbook 2001*)

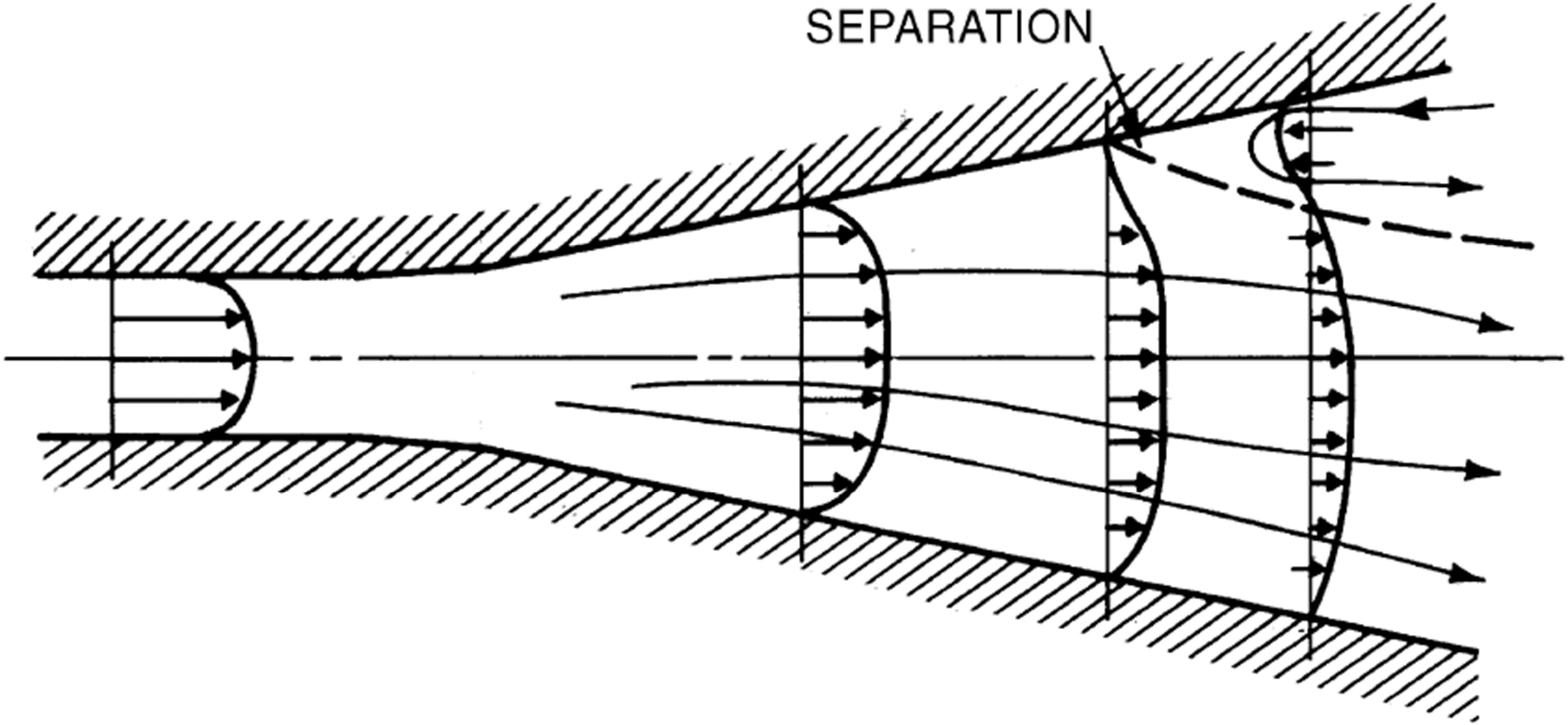


Examples of geometric separation in flows in conduits

(Source: *ASHRAE Fundamentals Handbook 2001*)

Basic Flow Processes

- Flow separation in diffuser
  - To expand a flow efficiently, the device shall be designed with gradual contours, a diffuser, or a rounded entrance
  - To control separation
    - May use splitters to divide the diffuser into smaller divisions less likely to have separations
    - May bleed some low-velocity fluid near the wall



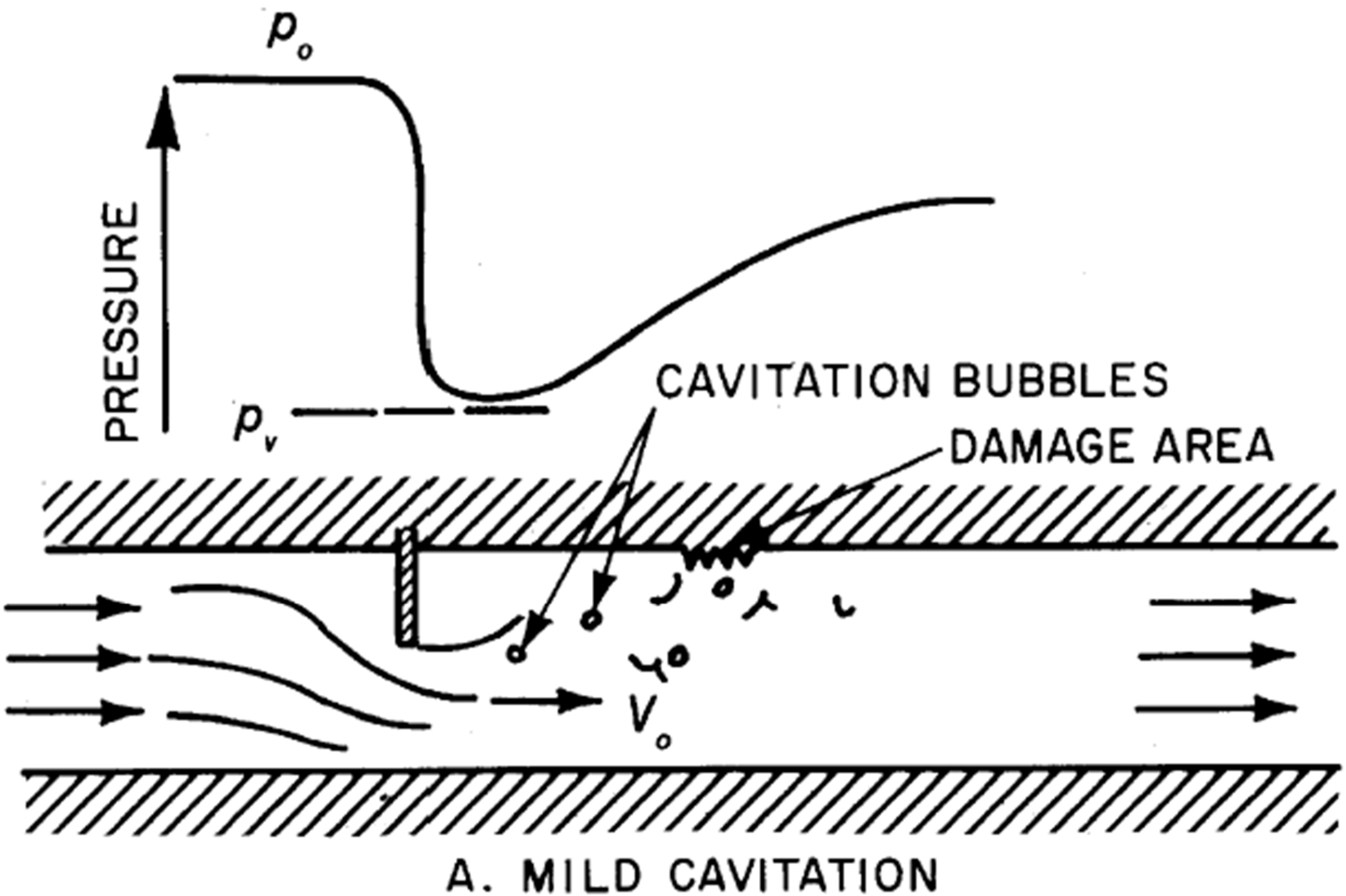
Separation in flows in diffuser

(Source: *ASHRAE Fundamentals Handbook 2001*)

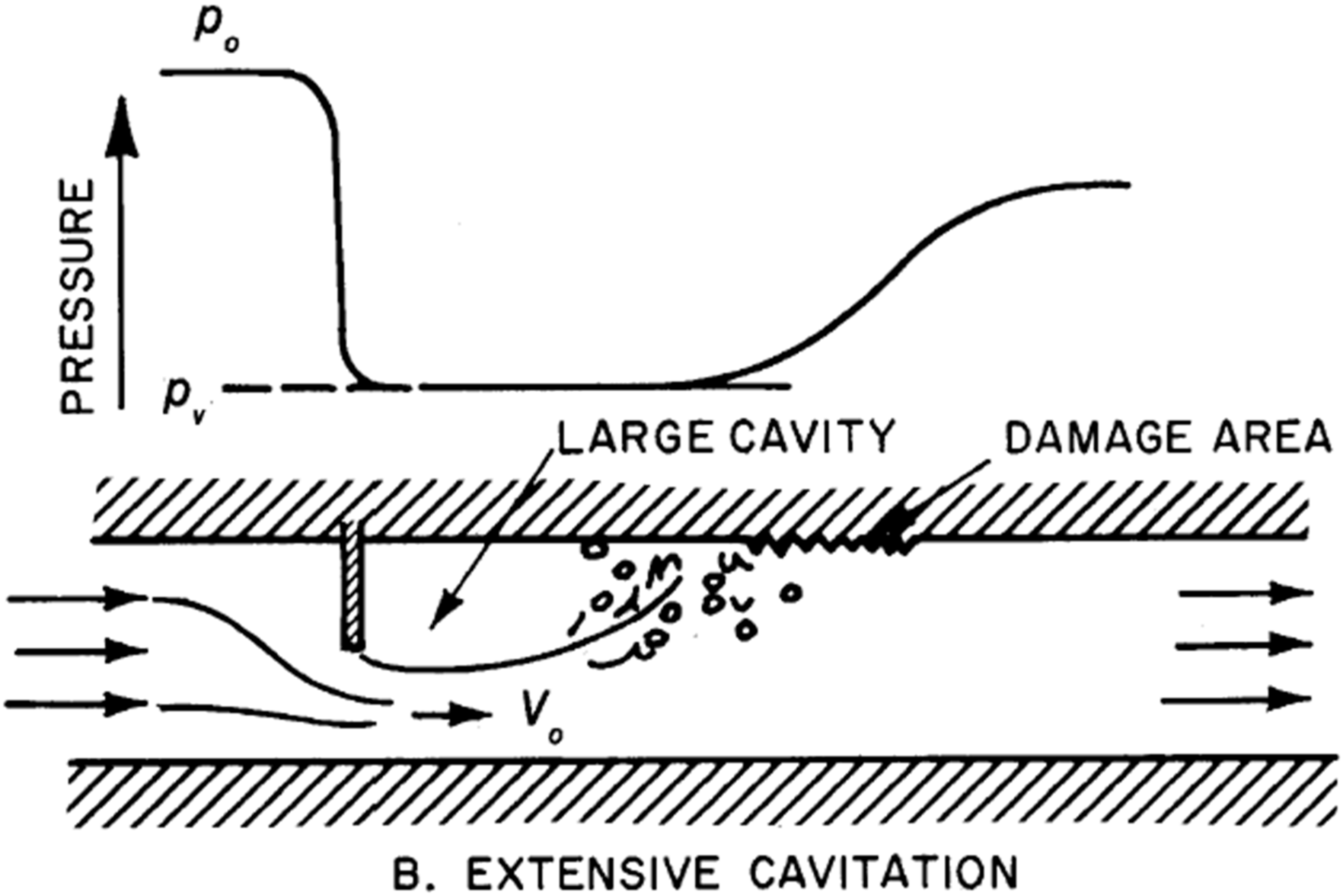
Basic Flow Processes

- Cavitation*
  - Liquid flow with gas- or vapour-filled pockets can occur if the absolute pressure is reduced to vapour pressure or less
    - Collapse noise of many small bubbles
    - More bubbles appear & may join to form large cavities
    - May modify flow pattern & alter device performance
    - Frequent collapse of cavities on or near solid boundaries may result in damage through cavitational erosion or excessive vibration

* See also http://en.wikipedia.org/wiki/Cavitation



(Source: *ASHRAE Fundamentals Handbook 2001*)



(Source: *ASHRAE Fundamentals Handbook 2001*)

Basic Flow Processes

- Methods to avoid cavitation
  - 1. Operate the device at high enough pressure
  - 2. Change the flow
  - 3. Device is built to withstand the cavitation effects (e.g. by surface coating)
  - 4. Design surface contours to delay the advent of cavitation

Flow Analysis

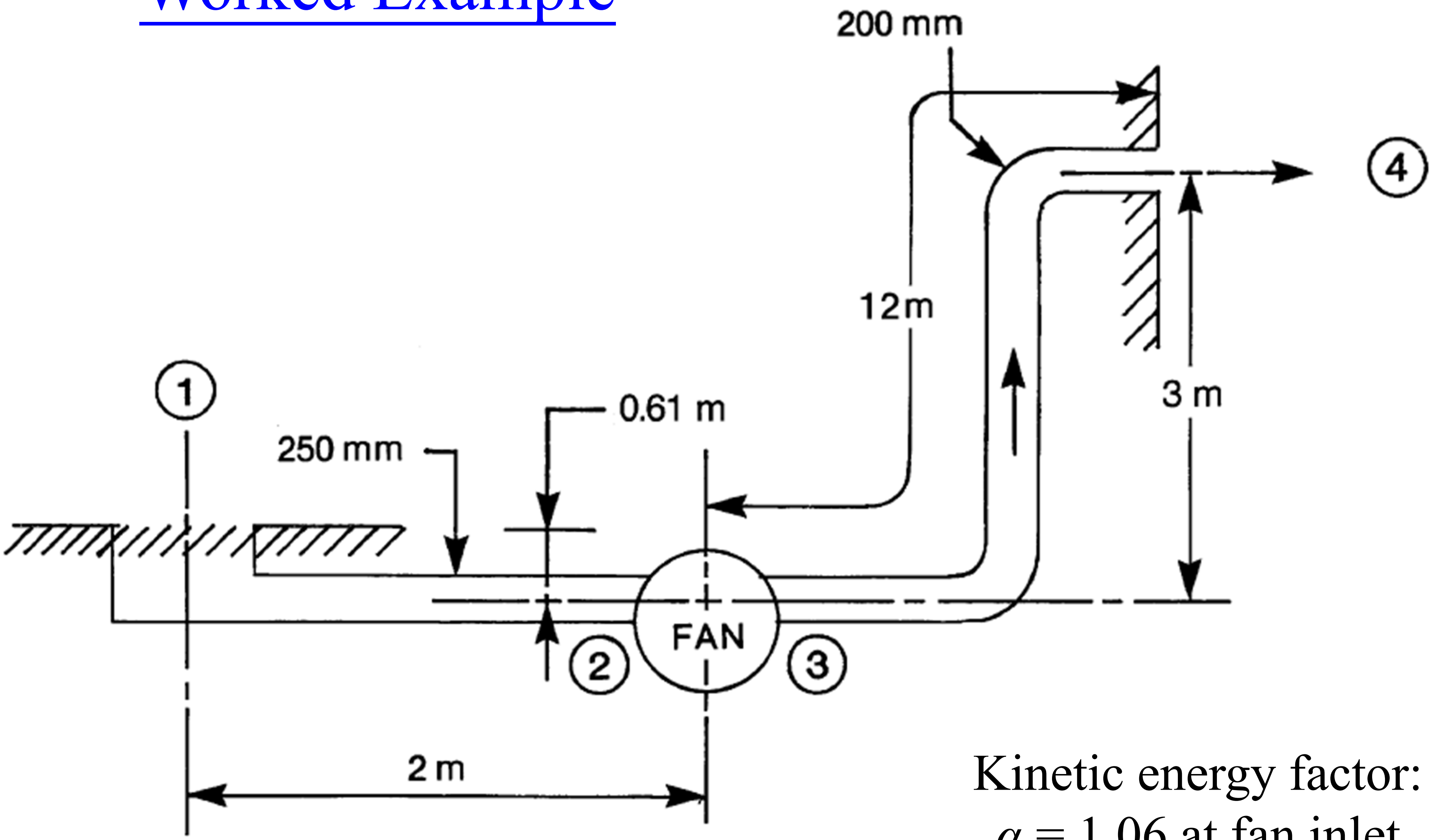
- Aims
  - To correlate pressure changes with flow rates and nature of the conduit
  - To evaluate flow rate and specify pump/fan for a conduit piping system
- Generalised Bernoulli Equation

$$\left(\frac{p}{\rho g}+\alpha\frac{V^2}{2g}+z\right)_1+H_M=\left(\frac{p}{\rho g}+\alpha\frac{V^2}{2g}+z\right)_2+H_L$$

Flow Analysis

- Worked Example:
  - Specify the fan to produce an isothermal airflow of 200 L/s through the ducting system. Accounting for intake and fitting losses, the equivalent conduit lengths are 18 and 50 m and the flow is isothermal. The pressure at the inlet (station 1) and following the discharge (station 4), where the velocity is zero, are the same. Friction losses H_L are evaluated as 7.5 m of air between stations 1 and 2, and 72.3 m between stations 3 and 4.

Worked Example



Kinetic energy factor:

$\alpha = 1.06$ at fan inlet

$\alpha = 1.03$ at fan outlet

(Source: *ASHRAE Fundamentals Handbook 2001*)

Flow Analysis

- Apply Bernoulli equation to stations 1 & 4
  - The pressure terms are the same; velocity is zero
  - $(p/\rho g)+0+0.61+H_M = (p/\rho g)+0+3+(7.5+72.3)$
  - Therefore, $H_M = 82.2$ m of air = required fan pressure
- Alternatively, H_M can be determined from stations 2 & 3, but some more steps are needed, as shown in the followings

Flow Analysis

- Calculate the kinetic terms at fan inlet/outlet:
  - $A_2 = \pi(D/2)^2 = \pi(0.25/2)^2 = 0.0491\ \text{m}^2$
  - $V_2 = Q\ /\ A_2 = 0.2\ /\ 0.0491 = 4.07\ \text{m/s}$
  - For fan inlet, $V_2^{\,2}/2g = (4.07)^2\ /\ 2(9.8) = 0.846\ \text{m}$
  - Similarly for fan outlet, $V_3^{\,2}/2g = 2.07\ \text{m}$
- Apply Bernoulli to stations 1 & 2 and 3 & 4
  - $(p_1/\rho g)+0+0.61+0=(p_2/\rho g)+(1.06\text{x}0.846)+0+7.5$
  - $(p_3/\rho g)+(1.03\text{x}2.07)+0+0=(p_4/\rho g)+0+3+72.3$

Flow Analysis

- Therefore,
  - $(p_2/\rho g)-(p_1/\rho g) = -7.8$ m of air
  - $(p_3/\rho g)-(p_4/\rho g) = 73.2$ m of air
- Apply Bernoulli to stations 2 & 3 and knowing $p_1 = p_4 =$ zero gauge, therefore,
  - $H_M = 73.2 + (1.03\text{x}2.07) – [-7.8 + (1.06\text{x}0.846)] = 75.3 – (-6.9) =$ 82.2 m of air

Flow Analysis

- Conduit friction
  - Frictional shear at bounding walls
  - Flow energy is converted into heat (fluid internal energy), unrecoverable (a loss)
  - This loss can be evaluated by Darcy-Weishbach Equation:

$$(H_L)_f = f\left(\frac{L}{D}\right)\left(\frac{V^2}{2g}\right)$$

    - L = length of conduit
    - D = diameter
    - f = friction factor (for turbulent flow, f = 0.01 to 0.05)

Flow Analysis

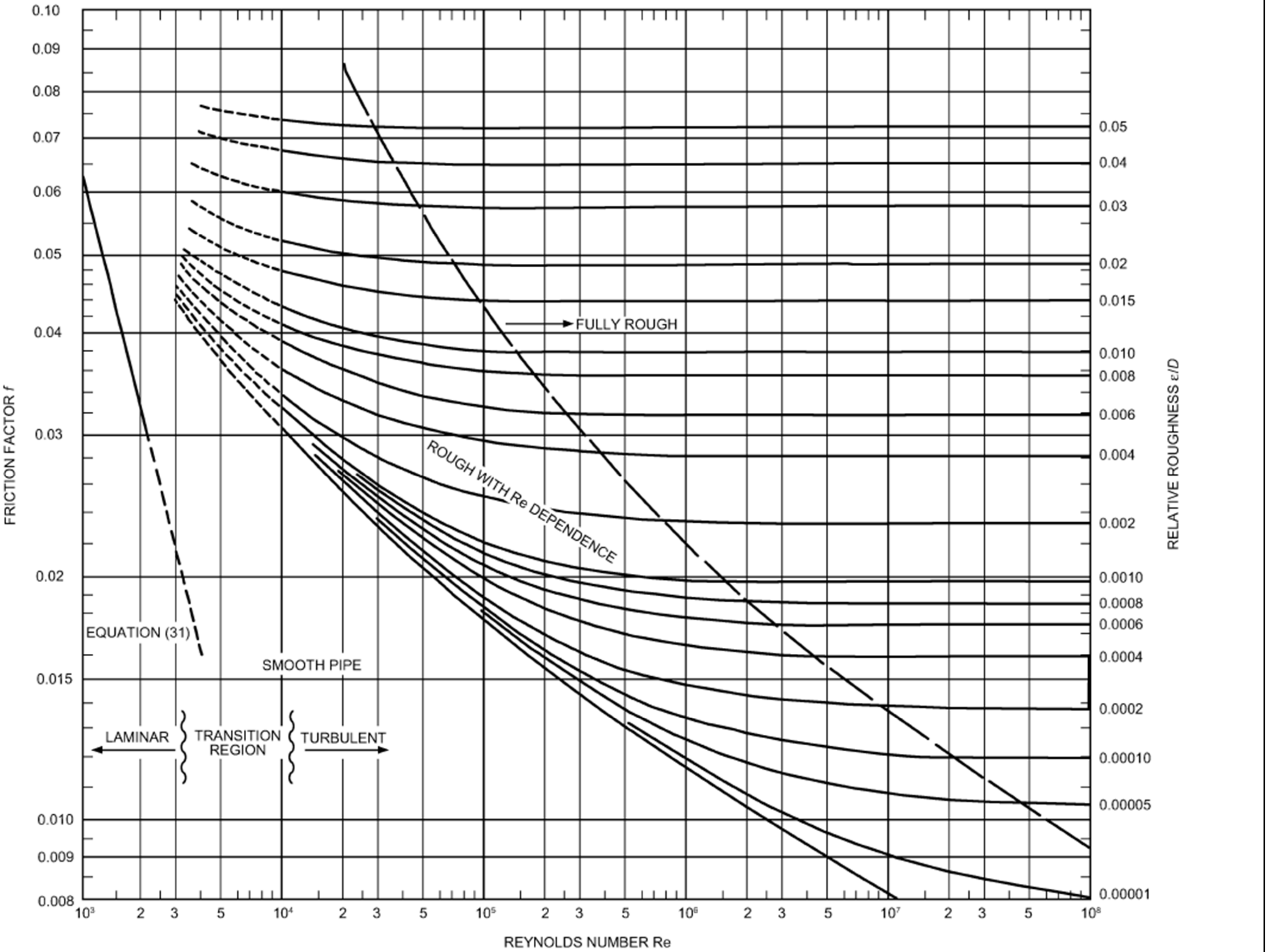
- For fully-developed laminar flow in a pipe,

$$\left(H_L\right)_f = \frac{L}{\rho g}\left(\frac{8\mu V}{R^2}\right) = \frac{32 L \nu V}{D^2 g} = \frac{64}{VD/\nu}\left(\frac{L}{D}\right)\left(\frac{V^2}{2g}\right)$$

  - Where Re = VD/ν and $f = 64$ / Re
  - Friction factor varies inversely with Re
- With turbulent flow, friction loss depends also on nature of conduit wall surface

Flow Analysis

- For smooth conduit walls, empirically,
  - $f = 0.3164 / Re^{0.25}$ for $Re < 10^5$
  - $f = 0.0032 + 0.221 / Re^{0.237}$ for $10^5 < Re < 3 \times 10^6$
- f also depends on wall roughness ε and cannot studied using a "Moody chart"
  - For high Re and ε, friction factor is independent of Re in a fully-rough flow regime, then
    - $1/\sqrt{f} = 1.14 + 2 \log (D/\varepsilon)$



(Source: *ASHRAE Fundamentals Handbook 2005*)

Flow Analysis

- Between smooth tubes and fully-rough regime, friction factor can be represented by Colebrook's natural roughness function:

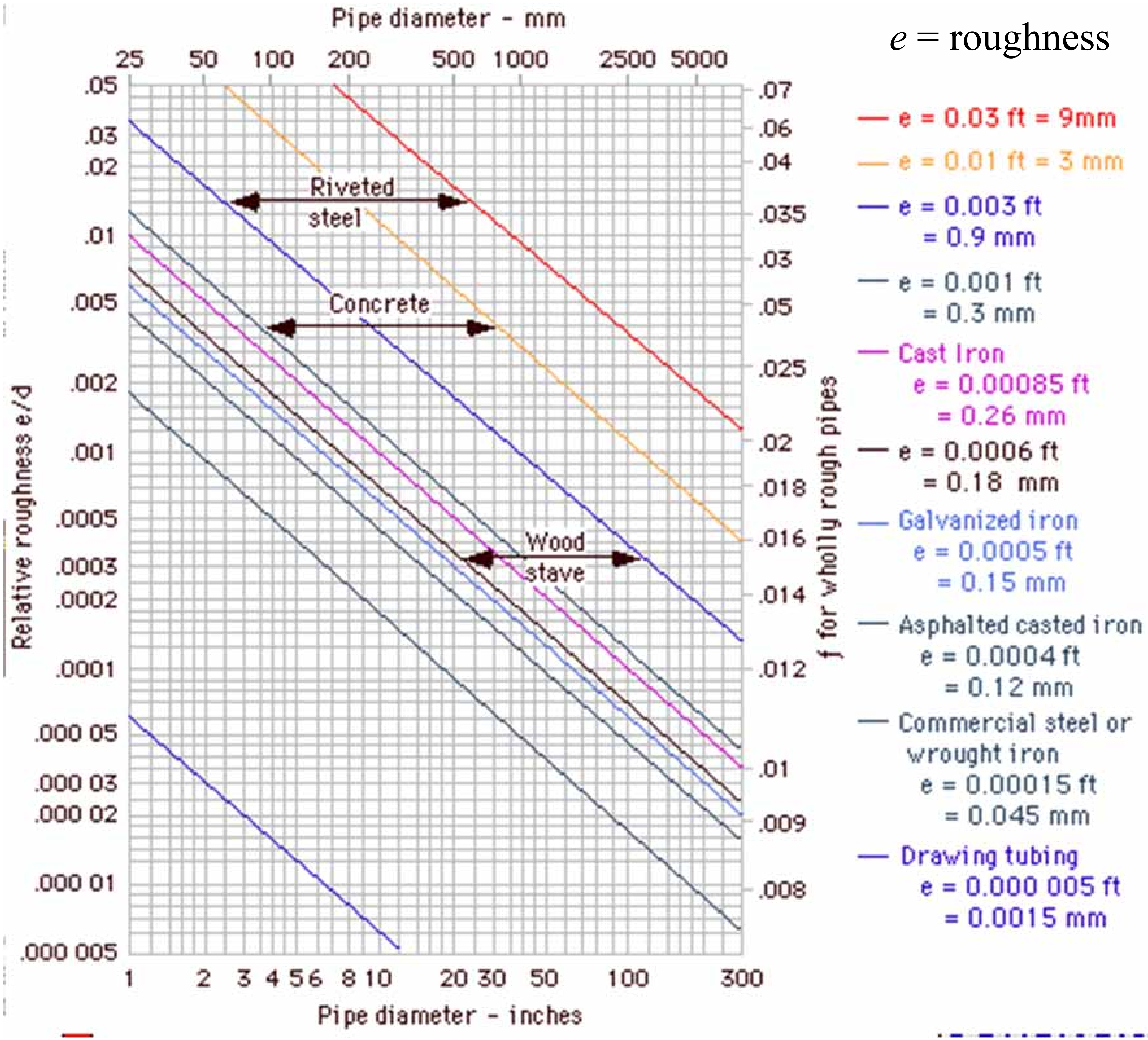
$$\frac{1}{\sqrt{f}} = 1.14 + 2\log(D/\varepsilon) - 2\log\left[1 + \frac{9.3}{\text{Re}(\varepsilon/D)\sqrt{f}}\right]$$

- Transition region: 2000 < Re < 10000
- For smooth wall,
  - Laminar: Re < 2000, $f = 64/\text{Re}$
  - If Re > 10000, the empirical equations are used

Flow Analysis

- For rough walls, Moody chart and Colebrook function are used to assess friction factor in turbulent flow
- The roughness height will be evaluated from the conduit surface (found from Table)
- For rectangular air duct, the circular equivalent can be calculated using $D_{\text{eq}} = 4A / P_w$
  - A = flow area; P_w = wetted perimeter of cross section

Pipe sizing chart



Further Reading

- ASHRAE, 2009. *ASHRAE Handbook Fundamentals 2009*, Chp. 3 - Fluid Flow, American Society of Heating, Refrigerating and Air-Conditioning Engineers Inc., Atlanta, GA. [ebook via Knovel] [ASHRAE catalog via Techstreet]

- Web Links:
  - CIVE1400: Fluid Mechanics [University of Leeds]
  - http://www.efm.leeds.ac.uk/CIVE/CIVE1400/course.html